Nitrogen-Rejecting Membranes to Increase Gas Heating Value and Recover Pipeline Natural Gas A Simple Wellhead Process Approach

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# Outline

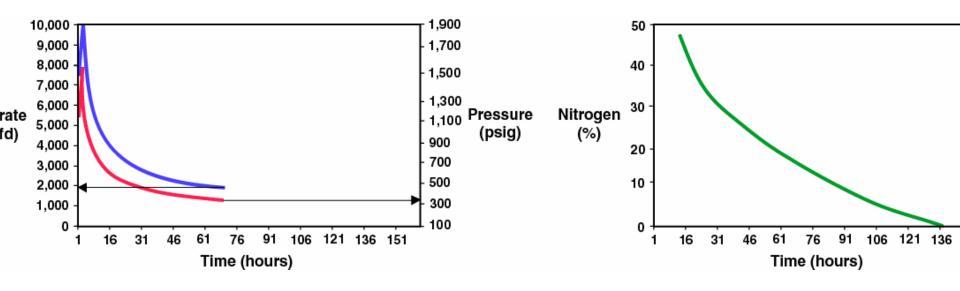
Application –

Recapturing CH<sub>4</sub> from Blow down of Nitrogen-Foam Fractured Horizontal and Vertical Wells.

- Novel Composite Membranes
- Why a Membrane Process for this Application ?
- Process Designs and Economics
- Conclusions

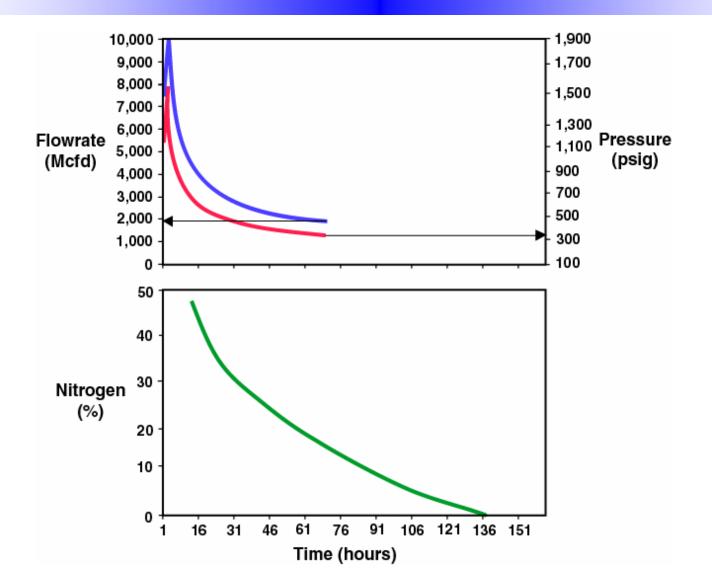


### High Rate Nitrogen-Rich Blowdown Operation in Nitrogen-Foam Fractured Horizontal Wells



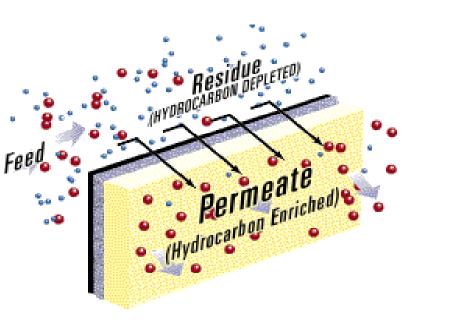


### High Rate Nitrogen-Rich Blowdown Operation in Nitrogen-Foam Fractured Horizontal Wells





### **Membrane Separation Mechanism**



MTR's Rubbery Membranes Reject Nitrogen and Permeate Hydrocarbon Components A membrane can separate components of a gas mixture due to differential permeation rates across a non-porous polymer film resulting in a differential pressure driving force.

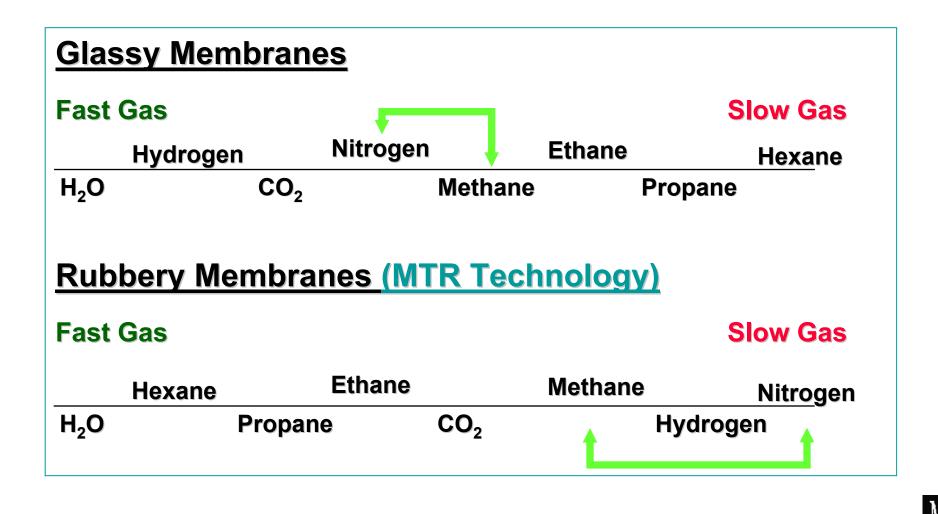
Permeability = Diffusivity \* Solubil (P) (D) (S)

**Membrane Selectivity** 

 $\frac{P_{1}}{P_{2}} = \frac{D_{1}}{D_{2}} \cdot \frac{S_{1}}{S_{2}}$ 



## **Glassy versus Rubbery Membranes**



### Membrane System Installations Membranes are a Mature Separation Technology

### **Gas/Gas Separation Systems**

 $H_2/N_2$ ,  $CH_4$  ~ 200 Units

  $O_2/N_2$  ~ 5,000 Units

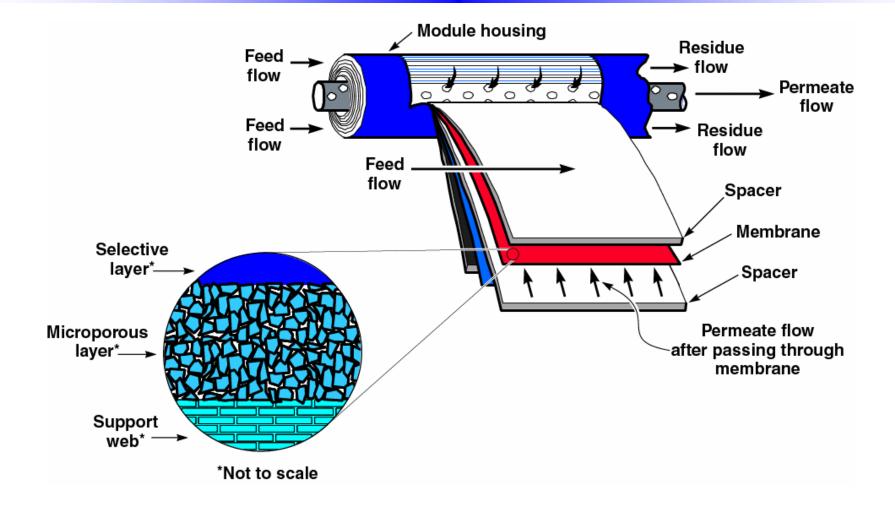
  $CO_2/CH_4$  ~ 200 Units

Vapor/Gas Separation Systems (MTR'S Reference Base)

Hydrocarbon/N<sub>2</sub>,  $CH_4 \sim 100$  Units



## MTR Membrane in Spiral Wound Cartridges





## **Typical Commercial Skid-Mounted Unit**



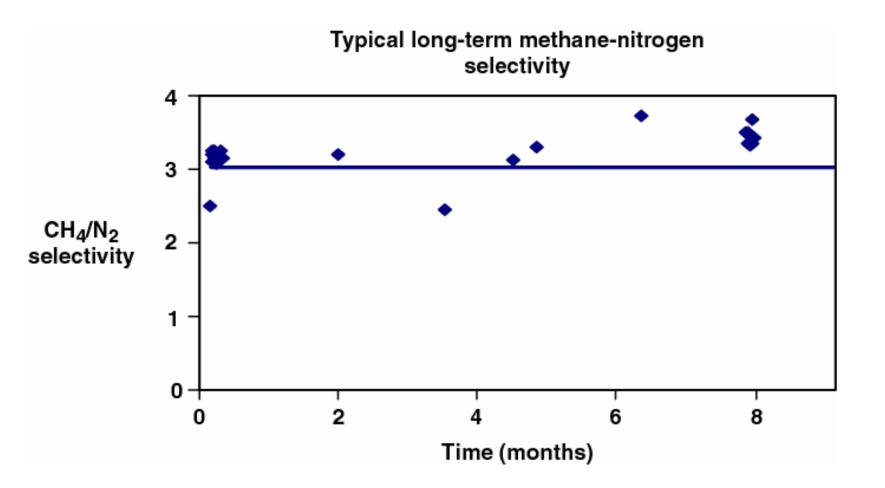
Twin Bottoms Membrane System Design Flow Rate-0.2 MMSCFD



NTE Membrane System Design Flow Rate-1.0 MMSCFD



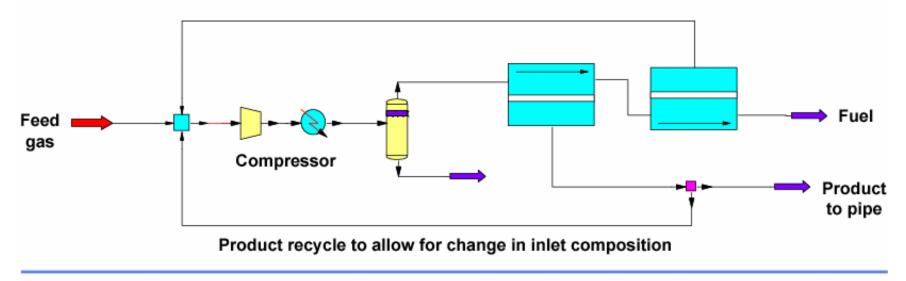
Proven Long-Term Separation Efficiency (400 years Cumulative Operating Experience with Silicone Rubber Membrane)





### **Process Flow Diagram for Vertical Wells**

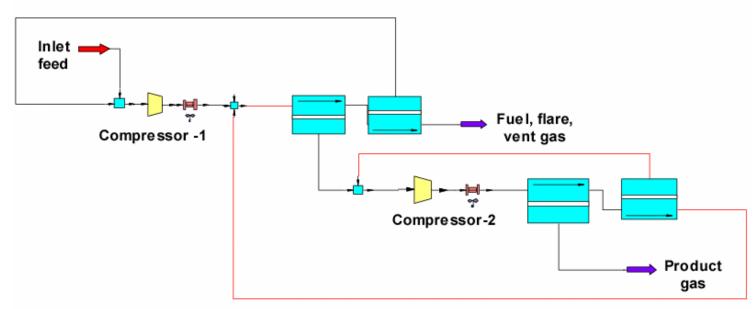
15% inlet nitrogen content < 4 mol% product nitrogen content Btu enhancement from 830 to 970 Btu/scf



Feed gas flow rate:	0.500 MMSCFD
Feed gas nitrogen content:	15 mol%
Pipeline gas nitrogen content:	4 mol%
Annual net revenue:	\$US 600,000
Annual operating expenses:	\$US 165,000
Simple payback period:	9 months
Membrane system price:	\$US 350,000

### Process Scheme for High Nitrogen Feed Gas from Horizontal Wells

12-30 mol% nitrogen in inlet gas < 4 mol% nitrogen in product gas Btu enhancement from 783 to 890 Btu/scf



Feed gas flow rate:	3.5 MMSCFD
Feed gas nitrogen content:	31 mol%
Pipeline gas nitrogen content:	10 mol%
Annual net revenue:	\$US 3.5 million
Annual operating expenses:	\$US 515,000
Simple payback period:	6 months
Membrane system price:	\$US 620,000 - 720,000



## Nitrogen Rejection – Application Envelope

- Inlet nitrogen content between 4 and 30 vol%
- Inlet flow rate between 0.1 20 MMSCFD
- Discharge N<sub>2</sub> specification between 4 and 8 vol%
- Upgrading to pipeline acceptability
- Upgrading fuel gas to meet heating value for burning
- Hydrocarbon removal for nitrogen re-injection
- Mobile units can be manufactured easily



- Simple passive system
- High on-stream factor (typically > 98%)
- Minimal or no operator attention
- Small footprint, low weight
- Large turndown ratio
- Low maintenance
- Lower capital and operating costs
- Units are mobile. No foundation required. Level gravel or soil is adequate for membrane skid.



Other Applications in the Oil & Gas Industries for MTR's Reverse-Selective Membranes

- Gas: Fuel gas conditioning NG Dew point Control NGL recovery Natural gas dehydration.
- Oil: Associated gas processing Vapor recovery from storage tanks and ship vents.

